

# Conversion of Existing Hydrocarbon Pipelines for Hydrogen Service





# Build VS. Buy

## FOR

- **Cost** – new transmission line averages \$694,000 per km.
- **Easements** – major issue in industrial/urban areas
- **Schedule** – months vs. years

## AGAINST

- **Material** – will not match “ideal” H<sub>2</sub> compatibility
- **Corrosion** – old pipelines, several fluids, corrosion?
- **Risk concerns** – wall thickness, location, population

# U.S. Pipeline Inventory

- 483,000 Km. Natural Gas Transmission
- 217,000 Km. Oil & Products Transmission
- 45,000 Km. Natural Gas Gathering
- 34,000 Crude Oil Gathering
- Diminishing oil production, many underutilized lines
- Oil pipelines more available than natural gas

# Evaluation – 7 Steps

1. **Technical Documentation & Service History**
2. **Review of Legal Documentation** - Easements & Permits
3. **Visual Inspection** - walk the route
4. **Physical Inspection** - C.P. readings, depth of cover
5. **External Inspection** - excavate, check wall thickness
6. **Internal Inspection** - pressure test, “smart pig” inspection
7. **Risk Evaluation based on above data**

# Documentation and Legal

- **Purchasing Data** – pipe specs., welding specs, when built
- **Mill test reports** – chemistry, tensiles, charpy impact
- **Service History** – oil, gas, contaminants
- **Annual Cathodic Protection Survey** – 850ma?
- **History of leaks and repairs**
- **Integrity Management data** – hydrotest, internal inspection
- **Easements** – product specific?

- Original certificates may be missing
- Pipeline may be in service
- On-line techniques > hot tap coupon, P.M.I. methods
- Need chemistry, tensiles, Charpy Impact data



# Valves and Flanges

- Oil and natural gas valves may not hold hydrogen
- Replace flange connections with butt welds where possible
- Refurbish valves, refinish old flange faces
- Minimize compression tube fittings



# Pressure Test and Internal Tool Inspection

- Hydrotest usually required for change of service
- Tool inspection required if pipeline condition is a concern
- Need to know minimum wall thickness for MOP

- Acquire a population count along the route
- Evaluate potential damage from fire and detonation
- Risk calculations may indicate need for mitigation measures
- Metallurgy may require de-rating MOP <30 SMYS ?

# Carbon Steel Properties for H2

	<b>2005 IDEAL</b>	<b>1970's API 5L</b>	<b>1940's Grade B</b>
Hardness	<250 HB	225	178
Carbon Equivalent	<0.43	0.63	0.325
Grade	<X56	X60	Gr.B
Sulphur	<0.01%	0.03	0.036
Phosphorus	<0.015%	0.03	0.011
Charpy Impact	>35J	>27J	6J
Heat treatment	Normalized	NA	NA

# Conclusion

- Existing pipelines have been successfully converted to H2
- Needs careful metallurgical and risk analysis
- Cost is far lower than building new
- Conversion will be a major factor in the H2 infrastructure

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